

OPTIMIZATION OF XYLANASE PRODUCTION BY NEWLY ISOLATED STRAIN *TRICHODERMA AFROHARZIANUM* ISOLATE AZ 12 IN SOLID STATE FERMENTATION USING RESPONSE SURFACE METHODOLOGY

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Xylanases are hydrolytic enzymes with wide applications in several industries, such as biofuels, paper, deinking, food and feed. Response surface methodology and Box-Behnken matrix were used to optimize the culture conditions for xylanase production by *Trichoderma afroharzianum* isolate AZ 12 in solid state fermentation using wheat bran as substrate. The influence of four variables was examined in this research, namely incubation time, humidity, temperature and inoculum size. The analysis of variance was applied and xylanase production was expressed with a mathematical equation as a function of the factors. The optimal conditions for xylanase production were obtained as follows: 6 days of fermentation, humidity of 85%, incubation temperature of 22 °C and inoculum size of 1.9×10^7 spores/mL – under such conditions, xylanase activity increased from 8475.87 to 14766.28 U/mL. Experimental design has proven to be an effective method for determining the optimal parameters for enzyme production.

Keywords: hemicelluloses, fungus, Box-Behnken, wheat bran, fermentation

INTRODUCTION

A significant amount of hemicellulosic biomass is present in agricultural by-products. Such biomass is made up of various hemicellulosic polymers, such as xylan, mannan and galactans. Among them, xylan has drawn much interest.^{1,2} Complete xylan degradation requires the combined action of different xylanolytic enzymes, such as endo-xylanase, β -xylosidase, α -arabinofuranosidase and esterase.^{3,4}

Xylanase enzymes are produced by various bacteria of the *Bacillus* genus,^{5,6} fungi, such as *Aspergillus* and *Trichoderma*,^{1,7} and by yeasts.⁸ The products of xylan hydrolysis are xylose, xylobiose, xylotriose, xylotetrose and xylooligosaccharides. These compounds have possible applications as food additives for poultry, in wheat flour for improving dough handling and the quality of baked products, for extraction of coffee and plant oils, and, in combination with pectinase and cellulase, for the clarification of fruit juices and wines.⁹ Xylanase has been used in

bleaching during paper production, resulting in reduced use of chemicals.

The optimization of culture conditions by the classical one-factor-at-a-time approach needs a considerable amount of time and work. An alternative – the statistical strategy – is to use factorial experimental design and response surface methodology (RSM), which involves a minimum number of experiments and covers a large number of factors. These methods have also been employed to improve the microbial xylanase production in solid culture. There are many reports of studies based on the application of RSM in biotechnological processes.¹⁰⁻¹²

Therefore, this study was primarily designed to optimize selected process parameters for xylanase production by a new strain of *Trichoderma afroharzianum* (strain AZ 12) cultivated on wheat bran, in solid fermentation, using the RSM approach.

EXPERIMENTAL

Microorganism

Trichoderma afroharzianum isolate AZ 12 was used in this study. This strain was isolated decaying olive tree roots in the soil, in Akbou area, Bejaia, located in the north-east of Algeria. It was selected as a potent producer of xylanase and was cultured on potato dextrose agar medium at 28 °C for 7 days.

Trichoderma afroharzianum isolate AZ 12 was identified according to its morphological characteristics (separation of mycelium, shape, form, diameter and texture of spores/conidia) and the fungal spores were examined and studied using standard keys,¹³ combined with sequence data of their Internal Transcribed Spacer rDNA region (ITS), and genomic DNA was extracted according to Vazquez-Angulo.¹⁴ PCR amplification of ITS1-5.8S rDNA-ITS4 regions was performed by using universal primers ITS1 (5'-TCCGTAGGTGAACCTGCGG-3') and ITS4 (5'-TCCTCCGCTTATTGATATGC-3'),¹⁵ The PCR analysis was performed according to the method described by Gonzalez-Mendoza.¹⁶ Sequence data obtained in this study were subjected to a BLAST search of the NCBI non-redundant nucleotide database. Evolutionary analyses were performed using MEGA7 software. If the similarity of the sequence of the ITS region was more than 99% between a studied strain and its nearest neighbor, the strain concerned was considered to be the same species as its nearest neighbor.

A spore suspension (spore/mL) of *Trichoderma afroharzianum* isolate AZ 12 was prepared by growing this strain in PDA medium and was incubated at 28 °C for 7 days. Then, to count the spores, they were scraped delicately, to prevent detachment of the mycelium, with a sterile scraper, adding 10 mL of sterile distilled water containing 1% (v/v) Tween 80, and then collected in sterilized bottles to be used as inoculums for enzyme production. The suspension was diluted by 1:100 (v/v) and the spore count was performed in a counting chamber (Malassez REF 06 106 10 MARIENFELD, Germany).^{17,18}

Production of xylanase

Trichoderma afroharzianum isolate AZ 12 was cultivated using solid state fermentation (SSF) in a 500 mL flask, containing wheat bran (10 g) dry substrates moistened with modified Mandels medium¹⁹ with the following composition per liter: K₂HPO₄ 2 g, (NH₄)₂SO₄ 1.4 g, urea 0.3 g, MgSO₄ (7H₂O) 0.3 g, CaCl₂ 0.3 g, FeSO₄ (7H₂O) 5 mg, MnSO₄ (H₂O) 1.56 mg, ZnSO₄ (7H₂O) 1.4 mg and CoCl₂ 2 mg in distilled water. The pH of the medium was adjusted to 5, and it was sterilized at 121 °C for 20 min. An inoculum (spores/g) of *Trichoderma afroharzianum* isolate AZ 12 was seeded in a 500 mL flask and incubated at different temperatures. Thereafter, the enzymatic extracts were harvested by crushing the contents of the flasks in 100 mL of distilled water with a glass rod and

then shaking on an orbital shaker at 100 rpm for 10 min at room temperature. The filtrate was centrifuged at 10 000 g for 10 min at 4 °C. The clear supernatant was assayed for xylanase activity and stored at 4 °C until use.²⁰ For optimization studies, the composition of the culture medium was varied according to the experimental data, while the pH and source of carbon (wheat bran) were constant.

Xylanase assay

The xylanase activity was determined according to Bailey,²¹ using birchwood xylan (Roth, Karlsruhe, Germany) as a substrate. The liberation of reducing sugars was estimated by the dinitro-salicylic-acid (DNS) method.²² A 100 µL culture supernatant was added to 900 µL of xylan solution (2%, pH 4.8, 50 mM sodium citrate buffer) and incubated at 50 °C. After 10 min, 1.5 mL of 3,5-dinitrosalicylic acid reagent was added to stop the reaction, and the amount of reducing sugars released in the reaction was estimated by measuring the absorbance at 540 nm,²² and compared to a standard curve of xylose (0 to 1 µmol/mL). One unit (1 UI) of xylanase activity is defined as the amount of enzyme required to release 1 µmol xylose per minute under the assay conditions.

Response surface methodology

Box-Behnken design (BBD) was selected as a suitable response surface method for optimizing the xylanase production of the solid state fermentation in order to achieve the maximal production. The incubation time (X₁), humidity (X₂), temperature (X₃) and inoculum size (X₄) were selected as independent variables. These parameters were studied at three levels: low (-1), middle (0), and high (+1), whereas the amount of obtained product was defined as the response. The values of low and high levels were established by the one-factor-at-a-time approach (data not shown), and shown in Table 1.

27 experiments with 3 replicates of the central point were employed (Table 2) to fit the polynomial model based on a BBD matrix that was generated using the Design-Expert® software version 11.0.5.0 (Stat-Ease Inc.), and was conducted to optimize the processes.

For each assay, SSF employed 10 g of wheat bran and the initial pH was adjusted to 5. The amount of moisture added to the wheat bran (X₂) (Table 1) was previously prepared by using the minimal medium. The material was uniformly distributed into 500 mL Erlenmeyer flasks and sterilized by autoclaving at 121 °C for 20 min. When the medium reached room temperature, a suspension of different inoculum size (spores/g) (X₄) was spread evenly over the surface of each sample, according to the levels presented in Table 1, and incubated for three levels of time (X₁), at different incubation temperatures (X₃), according to the predetermined levels (Table 1). Regression analysis of the data to fit a second-order polynomial equation

(quadratic model) was carried out according to the following general equation (Eq. 1), which was, then, used to predict the optimum conditions of the extraction process:

$$R = \beta_0 + \sum_{i=1}^n \beta_i X_i + \sum_{i=1}^n \beta_{ii} X_i^2 + \sum_{i=1}^n \sum_{j=1}^n \beta_{ij} X_i X_j + \varepsilon \quad (1)$$

where R represents the response surfaces, β_0 is the intercept term, β_i is the linear effect, β_{ii} is the square effect, β_{ij} is the interaction effect, while X_i , X_i^2 and $X_i X_j$ are linear variable, quadratic variable, and term for interaction of the variables, respectively, and “ ε ” is the residual associated to the experiments. The surface plots were plotted by varying the values of two factors and keeping the values of other factors constant at zero level. Equation (1) was used to optimize the values of the independent parameters for the response.

Table 1
Variables and their levels for the experimental Box-Behnken design (BBD)

Variable	Coded level of variable		
	-1	0	+1
Incubation time (days)	3	5	7
Humidity (%)	55	70	85
Temperature (°C)	22	26	30
Inoculum size (spore/g)	10 ⁶	10 ⁷	1.9 x 10 ⁷

The corneal tissue of the fungal hyphae was stained by lactophenol cotton blue dye.²³ Figure 1 b shows this strain on lactophenol cotton blue and staining reveals septate hyphae, conidiophores very branched, irregularly whorled with ramifications at right angles, attenuated ovoid and ellipsoidal phialides at the top directly inserted on the conidiophore and green conidia, this strain was identified as *Trichoderma* sp.

The small subunit ribosomal RNA gene of *Trichoderma afroharzianum* strain AZ 12 was amplified from bulk genomic DNA by PCR and analyzed. The alignment of this ITS fragment with all related sequences in the NCBI database by the BLASTN program showed that it was identical to those of strain *Trichoderma afroharzianum*. The results reported in this research for the nucleotide sequence of the 5.8S rRNA gene (534 bp) was deposited in the GenBank databases under accession number MT305752.

Optimization of xylanase production using RSM

RSM was used to optimize the filtered variables to improve the production of xylanase based on BBD.²⁴ The four input variables: incubation time, humidity, temperature and

Statistical analysis

The experimental results obtained by the BBD were analyzed by Design-Expert 11® software (Version 11.0.5.0., USA). For all analyzes, the difference was considered significant when p -value < 0.05 for a 95% confidence interval.

RESULTS AND DISCUSSION

Biochemical and molecular characterization of *Trichoderma afroharzianum* strain AZ 12

Trichoderma afroharzianum isolate AZ 12 grew at 28 °C and manifested green colonies, with white cottony aerial mycelium (Fig. 1 a). Microscopic morphology entailed the analysis of zoospores, basidiospores, and sporangiospores, these spores were further stained.

inoculum size, and the response xylanase activity with respect to their 27 different trials are listed in Table 3.

Analysis of real and predicted results

According to the results obtained by the BBD matrix (Table 3), run 7 showed the highest xylanase activity (14037.10 U/mL) after 5 days of incubation at 85% humidity and 26 °C, using an inoculum size of 10⁶ spores/g, while run 5 showed the minimum activity of 1461.82 U/mL of xylanase production under the following conditions: incubation period of 7 days, humidity of 70%, temperature of 30 °C and inoculum size of 10⁷ spores/g. Ghoshal,²⁵ Khusro,²⁶ Bagewadi,²⁷ Long²⁴ and Menezes²⁸ confirmed the influence of optimized parameters on the xylanase production.

Variance analysis for xylanolytic production (ANOVA)

Significance of the model

ANOVA data for the model are tabulated in Table 4. This analysis demonstrated that the model is highly significant with a p -value of 0.0003, while the model's F -value of 9.01 implies the model is significant. There is only a 0.03% chance that an F -value this large could occur due to noise. A p -value < 0.05 is considered to be significant,²⁹ the

low value of the model (p -value) of 0.0003, indicating that this quadratic model is statistically significant at 95% confidence level, this means

that the variables of the model have a significant effect on the R response.

Table 2
Experimental design of BBD matrix

Run	Incubation time (days)	Humidity (%)	Temperature (°C)	Inoculum size (spore/g)
1	5	55	22	10^7
2	5	70	22	10^6
3	3	70	26	1.9×10^7
4	5	70	26	10^7
5	7	70	30	10^7
6	3	70	22	10^7
7	5	85	26	10^6
8	3	55	26	10^7
9	5	70	30	10^6
10	7	70	26	10^6
11	7	85	26	10^7
12	3	70	30	10^7
13	7	70	22	10^7
14	3	85	26	10^7
15	5	85	26	1.9×10^7
16	5	70	26	10^7
17	5	70	22	1.9×10^7
18	5	55	26	1.9×10^7
19	7	55	26	10^7
20	5	55	26	10^6
21	5	55	30	10^7
22	5	85	22	10^7
23	7	70	26	1.9×10^7
24	5	70	26	10^7
25	5	85	30	10^7
26	3	70	26	10^6
27	5	70	30	1.9×10^7



Figure 1: Morphology of *Trichoderma afroharzianum* strain AZ 12 obtained from roots; a) top view of the *Trichoderma sp.* colony in PDA; b) Microscopic morphology with lactophenol cotton blue (100 \times)

These results are further confirmed by the lack of fit, with an F -value of 16.81, which implies there is a 5.74% chance that a lack of fit F -value could occur due to noise, and was not significant compared to the pure error.³⁰ According to Bezerra,³¹ significant regression and a non-significant lack of fit present in the model was

well fitted to the experiments. Based on this, the regression equation can be validated.³²

Determination of R^2 coefficient

According to Goupy,²⁹ R^2 is a statistical parameter, which indicates the validity of the model studied. The measurement of correlation

and the statistical significance of the model by the coefficient of determination R^2 is 0.913, close to 1 (Table 4), indicating that 91.3% of the variability of the response can be expressed by the model, which means that only 8.7% of the variability is not expressed. The R^2 of the model is greater than 90%, it can be seen that the model has a strong fitting ability,³³ and the value of the coefficient of adjusted determination, adjusted R^2 , of 0.81 (Table 4) confirms that the actual values are close to the predicted values.^{34,35} The validation

coefficient (CV) of 18.08% (Table 4) indicates that the experiments are reliable and accurate.²⁶ All these studies reflect the accuracy and applicability of RSM.³⁴ This correlation was confirmed by plotting the real value curve as a function of the predicted values (Fig. 2). According to Figure 2, the points are distributed around the regression line. The model hence is considered of sufficient quality,³⁵ there is 91.31% chance that it actually explains the measured variations in response.

Table 3
Results of real and predicted values obtained by BBD

Run	Xylanase activity, U/mL	
	Real values	Predicted values
1	8037.77	7651.71
2	8910	9531.25
3	3435.5	4148.94
4	6423.96	6669.09
5	1461.82	1005.31
6	3925.01	3250.96
7	14037.1	13292.66
8	4781.09	5725.87
9	6412.79	6454.61
10	5869.63	6456.87
11	11287.8	10172.87
12	5706.46	3956.52
13	6891.12	7510.50
14	7166.05	8261.40
15	12566.3	11612.08
16	7063.23	6669.09
17	7912.61	7700.67
18	8232.24	7846.07
19	6388.2	5122.74
20	9649.36	9473.00
21	5462.83	6732.09
22	13393.3	13424.73
23	3363.97	4994.22
24	6520.08	6669.09
25	6858	8544.73
26	6323.38	5993.81
27	5769.05	4977.68

Table 4
Analysis of the regression model

Source	<i>p</i> -value	<i>F</i> -value	Significance
Model	0.0003	9.01	significant
Lack of fit	0.0574	16.81	not significant
R^2		0.9131	
Adjusted R^2		0.81	
CV (%)		18.08	

Significance of factors effect

Linear effect

The *p*-value of the coefficients less than 0.05 indicates that the corresponding variable is significant.³² ANOVA test applied for each factor of the culture of *Trichoderma afroharzianum* isolate AZ 12 showed that the linear effects, namely humidity (X_2), temperature (X_3) and the inoculum size (X_4), have a probable value of 0.0003, 0.0022 and 0.0475, respectively (Table 5). They are statistically significant at 95% level of confidence, being important variables for high production of xylanases.

A higher than optimum humidity might decrease porosity and lower oxygen transfer, while a lower than optimum level might reduce solubility and the degradation of the substrate.³⁶ Nutrient availability might also influence xylanase activity at varying humidity level.^{20,28} For xylanase production, different values have been reported as the optimum humidity. For instance, the optimum humidity in the production of xylanase by *Aspergillus niger* was 43%, while this amount was 83% using *Paecilomyces thermophila*.^{37,38}

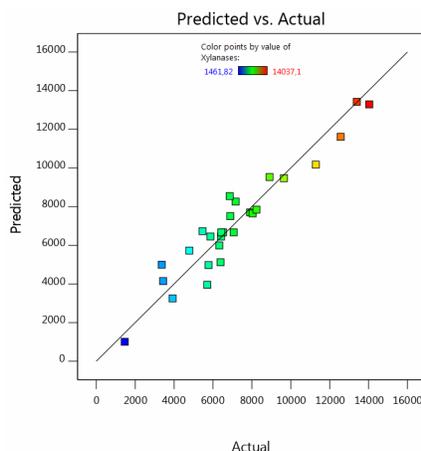


Figure 2: Correlation of actual and predicted values of xylanase activity by the response surface model

Table 5
ANOVA for response surface quadratic model (xylanase activity)

Source	<i>F</i> -value	<i>p</i> -value	Significance
X_1 -Time	0.7622	0.3998	not significant
X_2 -Humidity	25.62	0.0003	significant
X_3 -Temperature	14.98	0.0022	significant
X_4 -Inoculum size	4.87	0.0475	significant
X_1X_2	0.9385	0.3518	not significant
X_1X_3	7.72	0.0167	significant
X_1X_4	0.0217	0.8854	not significant
X_2X_3	2.33	0.1530	not significant
X_2X_4	0.0004	0.9839	not significant
X_3X_4	0.0186	0.8939	not significant
X_1^2	16.07	0.0017	significant
X_2^2	26.71	0.0002	significant
X_3^2	0.7458	0.4047	not significant
X_4^2	3.06	0.1060	not significant

Generally, humidity is an important factor affecting enzyme production. Low humidity reduces mass transfer and solubility of nutrients

and increases water tension, which decreases metabolic and enzymatic activity.³⁹ In contrast, high humidity decreases oxygen transfer and

porosity of the medium. It also changes the structure of substrate particles and clumps the medium affecting aeration and fungal growth.⁴⁰⁻⁴²

Many workers have reported different temperatures for maximum xylanase production. Abdel-Sater⁴³ screened xylan degrading filamentous fungi and reported that *T. harzianum* produced maximum xylanase at an incubation temperature of 35 °C. Goyal⁴⁴ reported the incubation temperature of 25 °C was best for xylanase production by *T. viride*. *Fusarium oxysporum* in shake flask cultures also produces maximum xylanase yield at an incubation temperature of 30 °C. Kuhad⁴⁵ and Javed⁴⁶ showed the maximal xylanase production from isolated strains *Aspergillus niger* at 30 °C. The optimum temperature of 40 °C was observed for xylanase production by *Aspergillus niger* via SSF.⁴⁷ These variations in incubation temperatures were due to the different nature of microorganisms and their environmental conditions. Since the fungal growth is affected by temperature, the enzyme product is dependent on temperature, but the physiological changes due to high temperatures in enzyme production are not well known. However, it is reported that high temperatures may limit the synthesis of essential proteins for fungal growth and other physiological processes.⁴⁸⁻⁵⁰

The small inoculum delays the biosynthesis of xylanases, which may be caused by the minimal presence of conidial cells, which are insufficient to use the fermentation medium in a better way.^{51,52} Generally, the maximum xylanase production was suggested when the inoculum size between 10⁶ and 10⁷ spores/mL.⁵³ Previous studies by Pathak,⁵⁴ Menezes²⁸ and Abd El Aty⁵⁵ on *Trichoderma harzianum*, *Aspergillus brasiliensis* and *Trichoderma longibrachiatum* KT693225, respectively, confirm the quote from Desai.⁵³

However, the incubation time impact is not significant, with a *p*-value of 0.3998 (Table 5). The results obtained are in agreement with those found by Zhang,⁵⁶ Xue,⁵⁷ Ramanjaneyulu,⁵⁸ and Yegin.⁵⁹ On the other hand, Okafor⁶⁰ isolated a strain of *Penicillium chrysogenum* PCL501 from wood wastes and reported that the highest xylanase activity of 6.47 U/mL was obtained with wheat bran after four days of fermentation. Abdel-Sater⁴³ obtained maximum production of xylanase from *Trichoderma harzianum* after 8

days of fermentation. Thomas⁵² achieved maximum enzyme production in 4 days of fermentation by *Aspergillus* sp. strain and Singh²⁰ reported maximum xylanase production of 722.98 and 228.62 U/mL for SH-1 and SH-2, respectively, increased up to seven days of incubation for both strains. According to Behnam,⁴⁸ short cultivation times provide conditions for the production of the economical enzymes. Generally, xylanase production increased with increasing time up to a certain level and then decreased, thus, cultivation time affects xylanase production by the fungi.

Interaction effect

In order to understand the effects of different factors and their interactions on the xylanase production, the results obtained showed that the interaction between X₁X₃ (incubation time and temperature) has a great influence on the enzymatic activity, with a *p*-value of 0.0167 (Table 5). By contrast, no significant interaction is observed between: X₁X₂ (time and humidity), X₁X₄ (time and inoculum size), X₂X₃ (humidity and temperature), X₂X₄ (humidity and inoculum size), X₃X₄ (temperature and inoculum size), with *p*-values of 0.3518, 0.8854, 0.1530, 0.9839, 0.8939, respectively (Table 5), which are greater than 0.05.

The relationship between the parameters and the responses can be understood by studying the three-dimensional (3D) response surface plots for xylanase activity; this response was generated from the predicted quadratic model. The 3D response surface plot can also be used to determine the optimum level of each variable for xylanase activity (Fig. 3 A-F). While maintaining other variables at their optimal level, the Z-axis (referring to xylanase activity) versus any two variables was constructed in the response surface plot.

Figure 3 A illustrates combinations of the effects of independent variables on the xylanase activity. From the data obtained from the surface response graph, a tendency can be observed of the xylanase activity as a function of X₁ and X₂ (Fig. 3 A) – these parameters influenced insignificantly xylanase production. Behnam⁴⁸ and Cao⁶¹ reported that the interaction term of moisture content and incubation time was insignificant in the optimization of xylanase production.

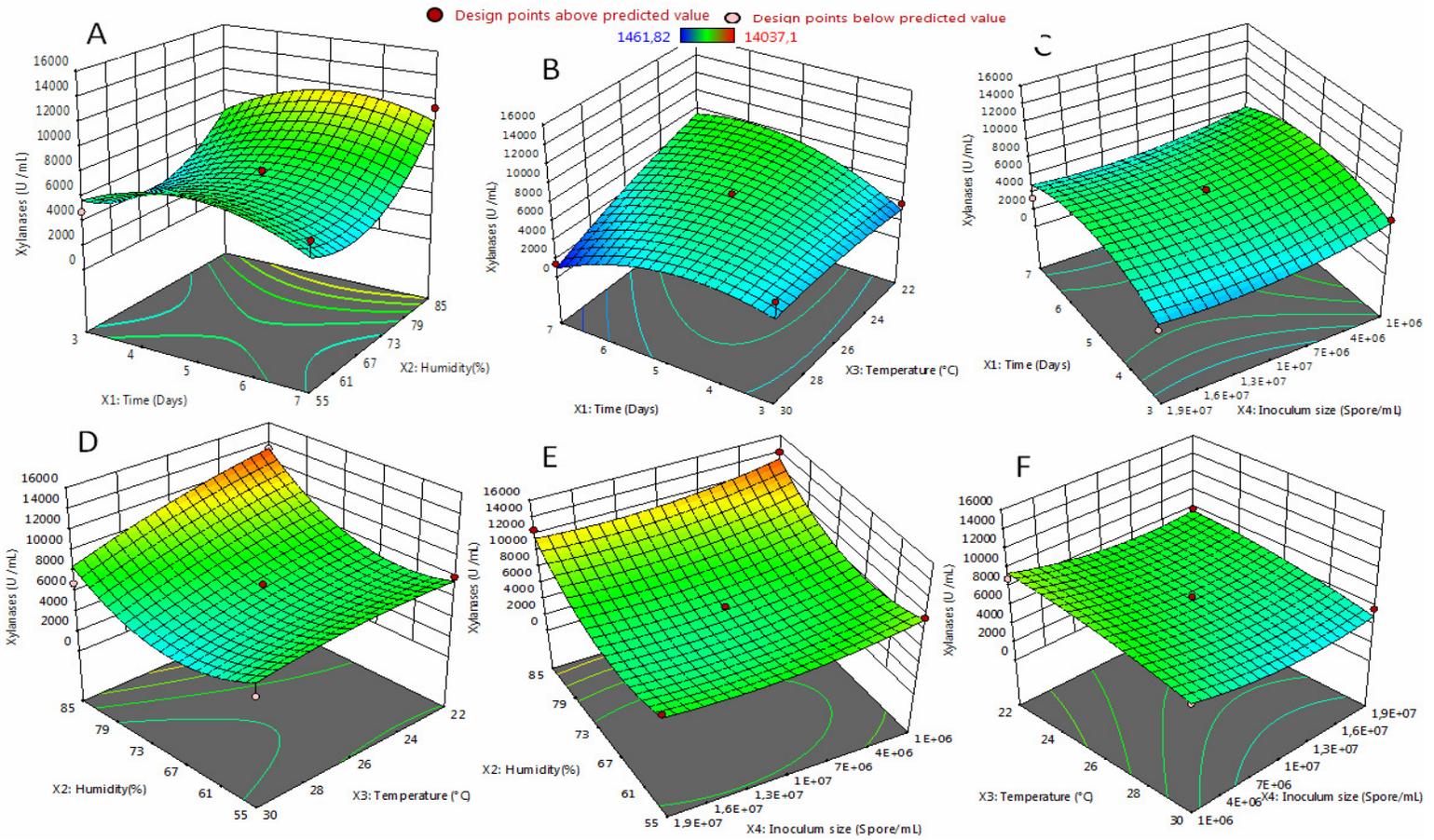


Figure 3: Response surface analysis for xylanase production by *Trichoderma afroharzianum* strain AZ 12 in solid state fermentation on wheat bran, with respect to incubation time and humidity (A), incubation temperature and incubation time (B), incubation time and inoculums size (C), humidity and incubation temperature (D), humidity and inoculums size (E) and incubation time and inoculums size (F)

Figure 3 B depicts the effect of X_1 and X_3 on the xylanase activity, when the humidity and inoculum size were fixed at level 0. The xylanase activity increased significantly ($p < 0.05$) with increasing the temperature and fermentation time, these parameters increase the xylanase activity, due to degradation of the polysaccharide molecules (xylan) present in the wheat bran by *Trichoderma afroharzianum* isolate AZ 12, and these two parameters may have influenced the metabolism responsible for xylanase production. The xylanase activity mainly depends on the temperature, as its quadratic and linear effects were highly significant (p -value of 0.002), confirming the single-factor experiment results (Table 5). Temperature is a very significant factor in the fermentation process; high and low temperature activity may result in the reduction of microbial growth and consequently lower the production of the enzyme. According to studies conducted by Yegin,⁶² Dos Santos,⁶³ Carvalho,⁶⁴ and Pathania,⁶⁵ the interaction between incubation time and temperature have an effect on xylanase production by strains *Aureobasidium pullulans* Y-2311-1, *Aspergillus niger*, and *Rhizopus delemar* F2, respectively. However, Behnam⁴⁸ reported that the interaction term of temperature and time was insignificant in the optimization of xylanase production by strain *Mucor indicus* through SSF.

Figures 3 C-F show the effects of X_1 and X_4 (Fig. 3 C), X_2 and X_3 (Fig. 3 D), X_2 and X_4 (Fig. 3 E) and X_3 and X_4 (Fig. 3 F) on the xylanase activity. These interactions are not significantly influenced by the response. It indicates an insignificant effect of the mutual interaction between these parameters. Behnam⁴⁸ and Cao⁶¹ reported that the interaction term of humidity and incubation time was insignificant in the optimization of xylanase production. On the other hand, the studies conducted by Hanly⁶⁶ reported that the interaction term of inoculum size and incubation time was significant in the

optimization of xylanase and cellulase production by strain *Terchoderma reesei*.

Quadratic effect

Quadratic effects of X_1^2 (incubation time x incubation time) and X_2^2 (humidity x humidity) have a p -value of 0.0017 and 0.0002, respectively, and are significant at 95% level. On the other hand, the terms X_3^2 (temperature x temperature) and X_4^2 (inoculum size x inoculum size) are statistically insignificant with a p -value of 0.4047 and 0.1060, respectively. Previously conducted studies by Narra,³⁴ Zhang,⁵⁶ Ping⁶⁷ and Rosmine⁶⁸ have found the quadratic parameters of incubation time and humidity are significant.

Mathematical regression model

The generated models were employed subsequently to study the effect of various parameters and their interactions on the xylanase activity, the model for the predicted response could be expressed by the quadratic polynomial equations (in the form of coded factors), they are excluded from the quadratic polynomial equation of the model.^{27,68} The simplified model is given by Equation (2) in terms of coded factors and can be used to make predictions about the response for given levels of each factor. The coded equation is useful for identifying the relative impact of the factors by comparing the factor coefficients.

$$R = 669.09 + 37.08X_1 + 1806.04X_2 - 152.25X_3 - 815.85X_4 + 628.65X_1X_2 - 182.69X_1X_3 + 95.55X_1X_4 - 87.47X_2X_3 - 13.41X_2X_4 + 55.32X_3X_4 - 277.85X_1^2 + 2970.95X_2^2 - 435.49X_3^2 + 940.83X_4^2 \quad (2)$$

where R is the xylanase activity, X_1 is incubation time, X_2 is humidity, X_3 is incubation temperature and X_4 is inoculum size. The positive sign in front of the terms indicates a synergistic effect, whereas the negative sign indicates an antagonistic effect on the xylanase enzyme product.

Table 6
Optimal conditions for xylanase production proposed by BBD model

Tests	Time (days)	Humidity (%)	Temperature (°C)	Inoculum size (spore/g)	Predicted values (U/mL)	Real values (U/mL)
1	5	85	29	1.6×10^7	9392.63	1355.09
2	6	85	22	1.9×10^7	14114.87	14766.28
3	7	85	22	1.9×10^7	14038.99	13352.52

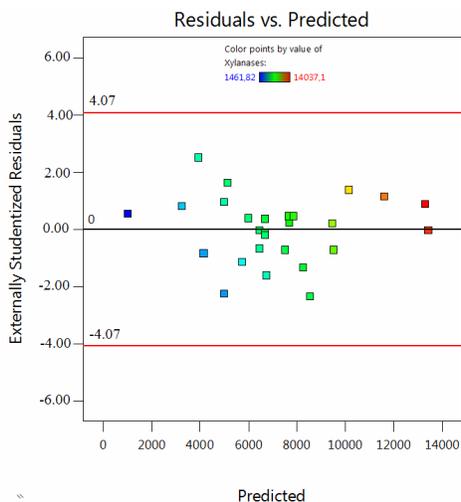


Figure 4: A residual plot for xylanase activity obtained by RSM

Model validation

Response surface equations were validated by the contrast between the experimental values and the estimated values derived from the response regression. The final step of the RSM after selecting the optimum parameter combination is to predict and verify the improvement of the performance characteristics with the selected optimum parameters. In this work, after determining the optimum conditions and predicting the response under these conditions, a new set of experiment was designed and conducted with the selected optimal conditions to predict and verify the accuracy of the mathematical model. A new range and level of the variables were studied in order to further determine the maximum xylanase production at different variable levels. The ranges of variable levels were set up based on the maximum production of xylanase recorded in the full model. The ranges of values used are shown in Table 6. The analysis of residuals appears to be a very useful and remarkably simple tool in model building and model criticism. Residuals play an important role in judging model adequacy. The residuals from the regression model are shown in Figure 4, which presents plot residuals *versus* the predicted response. A random pattern on these plots would indicate model adequacy.

The optimal conditions proposed by the BBD model for xylanase activity are shown in Table 6. The optimal xylanase production of 14766.28 U/mL was noted for test n° 2 under the following conditions: 6 days of incubation, 85% humidity, incubation temperature of 22 °C and inoculum size of 1.9×10^7 spores/g.

CONCLUSION

The current study elucidates potential xylanase production using wheat bran as economical carbon source by *Trichoderma afroharzianum* isolate AZ 12 in solid state fermentation. The statistical optimization method for the fermentation process can overcome the limitations of the classic empirical methods and proved to be a powerful tool for the optimization of xylanase production. The influences of different operating parameters (incubation time, humidity, incubation temperature and inoculum size) on xylanase production were studied by Box-Behnken matrix-based RSM. The study of 3D plots and ANOVA analysis of the quadratic model showed that the optimum xylanase production by *Trichoderma afroharzianum* strain AZ 12, employing wheat bran as solid substrate, was recorded at 14766.28 U/mL, for the following parameters of SSF: incubation temperature at 22 °C, 84% humidity, 6 days of fermentation and inoculum size of 1.9×10^7 spore/g. The applied second-order polynomial model gave a satisfactory description of the experimental data; it showed that the efficiency of xylanase activity was affected by the forth studied parameter. RSM was established to be more satisfactory and effective than other methods, due to its efficacy in studying many variables simultaneously, with a low number of experiments, saving time and costs.

REFERENCES

- 1 S. Shrivastava, V. Kumar, M. Baweja and P. Shukla, *J. Pure Appl. Microbiol.*, **10**, 2225 (2016), <https://go.gale.com/ps/i.do?id=GALE%7CA48165035>

3&sid=googleScholar&v=2.1&it=

r&linkaccess=abs&issn=09737510&p=AONE&sw=w

² M. Basu, V. Kumar and P. Shukla, *Curr. Protein Pept. Sci.*, **19**, 87 (2018), <http://dx.doi.org/10.2174/1389203718666161122110200>

³ S. Subramanian and P. Prema, *Crit. Rev. Biotechnol.*, **22**, 33 (2002), <https://doi.org/10.1080/07388550290789450>

⁴ T. Collins, C. Gerday and G. Feller, *FEMS Microbiol. Rev.*, **29**, 3 (2005), <https://doi.org/10.1016/j.femsre.2004.06.005>

⁵ C. Azeri, U. A. Tamer and M. Oskay, *African J. Biotechnol.*, **9**, 63 (2010), <https://www.ajol.info/index.php/ajb/article/view/77769>

⁶ B. Battan, J. Sharma, S. S. Dhiman and R. C. Kuhad, *Enzyme Microb. Technol.*, **41**, 733 (2007), <https://doi.org/10.1016/j.enzmictec.2007.06.006>

⁷ S. Kumar, N. Sharma and S. Pathania, *Cellulose Chem. Technol.*, **51**, 403 (2017), [http://www.cellulosechemtechnol.ro/pdf/CCT5-6\(2017\)/p.403-415.pdf](http://www.cellulosechemtechnol.ro/pdf/CCT5-6(2017)/p.403-415.pdf)

⁸ V. Lombard, H. Golaconda Ramulu, E. Drula, P. M. Coutinho and B. Henrissat, *Nucleic Acid. Res.*, **42**, 490 (2013), <https://doi.org/10.1093/nar/gkt1178>

⁹ P. Shukla, in “Frontier Discoveries and Innovations in Interdisciplinary Microbiology”, edited by V. Kumar and P. Shukla, Springer, New Delhi, 2015, pp. 157-165, https://doi.org/10.1007/978-81-322-2610-9_9

¹⁰ M. B. Limkar, S. V. Pawar and V. K. Rathod, *Biocatal. Agric. Biotechnol.*, **17**, 455 (2019), <https://doi.org/10.1016/j.bcab.2018.12.008>

¹¹ U. R. Ezeilo, R. A. Wahab and N. A. Mahat, *Renew. Energ.*, in press, (2019), <https://doi.org/10.1016/j.renene.2019.11.149>

¹² F. Yan, W. Lei, K. Ajab, Z. Rui, W. Siang *et al.*, *Poult. Sci.*, **99**, 263 (2020), <https://doi.org/10.3382/ps/pez482>

¹³ H. L. Barnett, and B. B. Hunter, “Illustrated Genera of Imperfect Fungi”, Burgers Publishing Company, Minneapolis, Minnesota, USA, 1972, pp. 241

¹⁴ J. C. Vazquez-Angulo, V. Mendez-Trujillo, D. González-Mendoza and A. Morales-Trejo, *Genet. Mol. Res.*, **11**, 1379 (2012), <http://dx.doi.org/10.4238/2012.May.15.8>

¹⁵ T. J. White, T. Bruns, S. Lee and J. Taylor, “PCR Protocols: A Guide to Methods and Applications”, Academic Press, San Diego, 1990, pp. 315-322, <https://www.researchgate.net/publication/223397588>

¹⁶ D. Gonzalez-Mendoza, A. Q. Moreno and O. Zapata-Perez, *Zeitschrift fur Naturforsch C*, **63**, 124 (2008), <https://doi.org/10.1515/znc-2008-1-222>

¹⁷ C. L. Handa, U. R. Couto, A. H. Vicensoti S. R. Georgetti and E. I. Ida, *Food Chem.*, **152**, 56 (2014), <http://dx.doi.org/10.1016/j.foodchem.2013.11.101>

¹⁸ S. K. Ang, A. Yahya, S. A. Aziz and M. Salleh, *Prep. Biochem. Biotechnol.*, **45**, 279 (2015), <https://doi.org/10.1080/10826068.2014.923443>

¹⁹ M. Mandels and J. Weber, *Food Microbiol.*, **23**, 391 (1969), <https://doi.org/10.1021/ba-1969-0095.ch023>

²⁰ S. Singh, C. H. Tyagi, D. Dutt and J. S. Upadhyaya, *New Biotechnol.*, **26**, 4 (2009), <https://doi.org/10.1016/j.nbt.2009.09.004>

²¹ M. J. Bailey, P. Biely and P. Kaisa, *J. Biotechnol.*, **23**, 257 (1992), [https://doi.org/10.1016/01681656\(92\)90074-j](https://doi.org/10.1016/01681656(92)90074-j)

²² G. L. Miller, *Anal. Chem.*, **31**, 426 (1959), <https://doi.org/10.1021/ac60147a030>

²³ D. Talukdar, R. Sharma, S. Jaglan, R. Vats, R. Kumar *et al.*, *Environ. Technol. Innov.*, **17**, 100604 (2020), <https://doi.org/10.1016/j.eti.2020.100604>

²⁴ C. Long, J. Liu, L. Gan, B. Zeng and M. Long, *Waste Biomass Valor.*, **10**, 1277 (2019), <https://doi.org/10.1007/s12649-017-0149-x>

²⁵ G. Ghoshal, U. C. Banerjee and U. S. Shivhare, *J. Biochem. Tech.*, **6**, 1013 (2016), <https://jbiochemtech.com/storage/models/article/FxtS9ecEME67kAMKR8qidsrs5a1b6tn8yttuS0bfPiYpTxP7zaMSVfTUfCPT/utilization-of-agrowaste-and-xylanase-production-in-solid-state-fermentation.pdf>

²⁶ A. Khusro, B. K. Kaliyan, N. A. Al-Dhabi, M. V. Arasu and P. Agastian, *Electron. J. Biotechnol.*, **22**, 16 (2016), <https://doi.org/10.1016/j.ejbt.2016.04.002>

²⁷ Z. K. Bagewadi, S. I. Mulla, Y. Shouche and H. Z. Ninnekar, *3 Biotech*, **6**, 164 (2016), <https://doi.org/10.1007/s13205-016-0484-9>

²⁸ S. Menezes, D. M. Rossi, F. Squina and A. Z. A. Marco, *Int. J. Food Sci. Technol.*, **53**, 2110 (2018), <https://doi.org/10.1111/ijfs.13798>

²⁹ J. Goupy, *Rev. Stat. Appl.*, **38**, 5 (1990), http://www.numdam.org/item/RSA_1990__38_4_5_0/

³⁰ M. Peña-Maravilla, M. Calixto-Romo, K. Guillén-Navarro, J. Sánchez and L. Amaya-Delgado, *Rev. Mex. Anal. Conducta*, **16**, 757 (2017), <http://www.redalyc.org/articulo.oa?id=62053304006>

³¹ M. A. Bezerra, R. E. Santelli, E. P. Oliveira, L. S. Villar and L. A. Escalera, *Talanta*, **76**, 965 (2008), <https://doi.org/10.1016/j.talanta.2008.05.019>

³² X. He, C. Song, Y. Li, N. Wang, L. Xu *et al.*, *Ecotoxicol. Environ. Saf.*, **150**, 232 (2018), <https://doi.org/10.1016/j.ecoenv.2017.12.043>

³³ Y. Xie, P. Hu, N. Zhu, F. Lei, L. Xing *et al.*, *Renew. Energ.*, **147**, 249 (2020), <https://doi.org/10.1016/j.renene.2019.08.109>

³⁴ M. Narra, G. Dixit, J. Divecha, K. Kumar, D. Madamwar *et al.*, *Int. Biodeter. Biodegrad.*, **88**, 150 (2014), <https://doi.org/10.1016/j.ibiod.2013.12.016>

³⁵ G. Coman and G. Bahrim, *Ann. Microbiol.*, **61**, 773 (2011), <https://doi.org/10.1007/s13213-0100195-0>

³⁶ M. Raimbault and D. Alazard, *Eur. J. Appl. Microbiol. Biotechnol.*, **9**, 199 (1980), <https://doi.org/10.1007/BF00504486>

³⁷ P. P. Kheng and I. C. Omar, *J. Sci. Technol.*, **27**, 325 (2005), <https://rdo.psu.ac.th/sjstweb/journal/27-2/10xylanase.pdf>

- ³⁸ S. Q. Yang, Q. J. Yan, Z. Q. Jiang, L. T. Li, H. M. Tian *et al.*, *Bioresour. Technol.*, **97**, 1794 (2006), <https://doi.org/10.1016/j.biortech.2005.09.007>
- ³⁹ A. K. Bharti, A. Kumar, A. Kumar and D. Dutt, *J. Radiat. Res. Appl. Sci.*, **11**, 271 (2018), <https://doi.org/10.1016/j.jrras.2018.01.003>
- ⁴⁰ K. Adinarayana, P. Ellaiah, B. Srini, R. Bha and G. Adinarayana, *Process Biochem.*, **38**, 1565 (2003), [https://doi.org/10.1016/S0032-9592\(03\)00057-8](https://doi.org/10.1016/S0032-9592(03)00057-8)
- ⁴¹ X. Wang, J. Bai and Y. Liang, *Appl. Microbiol. Biotechnol.*, **73**, 533 (2006), <https://doi.org/10.1007/s00253-006-0496-1>
- ⁴² M. Khanahmadi, I. Arezi, M. Amiri and M. Miranzadeh, *Biocatal. Agric. Biotechnol.*, **13**, 272 (2018), <https://doi.org/10.1016/j.bcab.2018.01.005>
- ⁴³ M. A. Abdel-Sater and A. H. M. El-Said, *Int. Biodeter. Biodegrad.*, **47**, 15 (2001), [https://doi.org/10.1016/S0964-8305\(00\)00113-X](https://doi.org/10.1016/S0964-8305(00)00113-X)
- ⁴⁴ M. Goyal, K. L. Kalra, V. K. Sareen, and G. Soni, *Brazilian J. Microbiol.*, **39**, 535 (2008), <https://doi.org/10.1590/S1517-83822008000300025>
- ⁴⁵ R. C. Kuhad, M. Manchanda and A. Singh, *Process Biochem.*, **33**, 641 (1998), [https://doi.org/10.1016/S0032-9592\(98\)00025-9](https://doi.org/10.1016/S0032-9592(98)00025-9)
- ⁴⁶ U. Javed, A. Aman, S. Ali and U. Qader, *Bioresour. Bioprocess.*, **4**, 1 (2017), <https://doi.org/10.1186/s40643-017-0149-5>
- ⁴⁷ A. Pal and F. Khanum, *Bioresour. Bioprocess.*, **101**, 7563 (2010), <https://doi.org/10.1016/j.biortech.2010.04.033>
- ⁴⁸ S. Behnam, K. Karimi, M. Khanahmadi and Z. Salimian, *Biol. J. Microorg.*, **4**, 1 (2016), <https://www.sid.ir/en/journal/ViewPaper.aspx?ID=509316>
- ⁴⁹ S. A. D. Harris and C. Ramalingam, *Asian J. Pharm.*, **9**, 50 (2016), <https://dx.doi.org/10.22377/ajp.v10i1.551>
- ⁵⁰ P. Kumar, B. Ryan and G. T. M. Henehan, *Protein Expr. Purif.*, **132**, 164 (2017), <https://doi.org/10.1016/j.pep.2017.01.011>
- ⁵¹ N. Bansal, R. Tewari, R. Soni and S. Kumar, *Waste Manag.*, **32**, 1341 (2012), <https://doi.org/10.1016/j.wasman.2012.03.006>
- ⁵² L. Thomas, B. Parameswaran and A. Pandey, *Renew. Energ.*, **98**, 9 (2016), <https://doi.org/10.1016/j.renene.2016.05.011>
- ⁵³ D. I. Desai and B. D. Iyer, *Waste Biomass Valor.*, **8**, 103 (2016), <https://doi.org/10.1007/s12649-016-9567-4>
- ⁵⁴ P. Pathak, N. K. Bhardwaj and A. K. Singh, *Appl. Biochem. Biotechnol.*, **172**, 3776 (2014), <https://doi.org/10.1007/s12010-014-0758-9>
- ⁵⁵ A. A. Abd El Aty, S. A. A. Saleh, B. M. Eid, N. A. Ibrahim and F. A. Mostafa, *Biocatal. Agric. Biotechnol.*, **14**, 129 (2018), <https://doi.org/10.1016/j.bcab.2018.02.011>
- ⁵⁶ H. Zhang and Q. Sang, *Biochem. Eng. J.*, **97**, 101 (2015), <https://doi.org/10.1016/j.bej.2015.02.014>
- ⁵⁷ J. Xue, S. Zhao, R. M. Liang, X. Yin, S. X. Jiang *et al.*, *Bioresour. Technol.*, **204**, 130 (2016), <https://doi.org/10.1016/j.biortech.2015.12.082>
- ⁵⁸ G. Ramanjaneyulu and B. R. Reddy, *Front. Microbiol.*, **7**, 1450 (2016), <https://doi.org/10.3389/fmicb.2016.01450>
- ⁵⁹ S. Yegin, *Prep. Biochem. Biotechnol.*, **47**, 441 (2017), <https://doi.org/10.1080/10826068.2016.1224245>
- ⁶⁰ U. A. Okafor and V. I. Okochi, *African J. Biotechnol.*, **6**, 1710 (2007), <https://www.ajol.info/index.php/ajb/article/view/57761>
- ⁶¹ Y. Cao, D. Meng, J. Lu and J. Long, *African J. Biotechnol.*, **7**, 631 (2008), <https://www.ajol.info/index.php/ajb/article/viewFile/58488/46832>
- ⁶² S. Yegin, A. Oguz, B. Sayit and S. Yekta, *Waste Biomass Valor.*, **8**, 999 (2016), <https://doi.org/10.1007/s12649-016-9646-6>
- ⁶³ T. C. dos Santos, N. dos Santos Reis, T. P. Silva, R. C. F. Bonomo, E. Aguiar-Oliveira *et al.*, *Waste Biomass Valor.*, **9**, 571 (2017), <https://doi.org/10.1007/s12649-016-9646-6>
- ⁶⁴ T. Carvalho, S. Reis, T. Pereira, J. Rangel and D. O. Marcelo, *Waste Biomass Valor.*, **9**, 571 (2017), <https://doi.org/10.1007/s12649-016-9810-z>
- ⁶⁵ S. Pathania, N. Sharma and S. Handa, *J. Pharmacogn. Phytochem.*, **6**, 1872 (2017), <http://www.phytojournal.com/archives/2017/vol6issue6/PartZ/6-6-183-481.pdf>
- ⁶⁶ L. Ping, M. Wang, X. Yuan, F. Cui, D. Huang *et al.*, *Int. J. Biol. Macromol.*, **109**, 1270 (2018), <https://doi.org/10.1016/j.ijbiomac.2017.11.130>
- ⁶⁷ E. Rosmine, N. C. Sainjan, R. Silvester, A. Alikunju and S. A. Varghese, *J. Genet. Eng. Biotechnol.*, **15**, 393 (2017), <https://doi.org/10.1016/j.jgeb.2017.06.001>
- ⁶⁸ M. Hosseinkhani, M. Montazer, S. Eskandarnejad and T. Harifi, *J. Nat. Fibers*, **14**, 175 (2017), <https://doi.org/10.1080/15440478.2016.1187702>