Preparation and Characterization of Ascorbic Acid Microcapsules Based on Gelatin Extracted from Tilapia Scale

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Gelatin extracted from tilapia scale (FSG) is used to encapsulate ascorbic acid under ultrasonic to demonstrate that FSG is a promising wall material in microencapsulation. The microcapsules are prepared with 15 mg/mL of gelatin and factors including concentration of transglutaminase and ascorbic acid, amount of emulsifier and temperature of solidification that related to the encapsulation rate are studied. Finally, the microcapsule with the highest encapsulation rate of 81.17 % is spheroid with average particle size of 5.73 μm . The ascorbic acid retention in the microcapsule is 53.39 % at 5 °C and 5.79 % at 25 °C after 30 days of storage. While at 37 °C, it is only 10 h, the encapsulation rate of ascorbic acid reaches 41.08 %. Thus, controlled-release without phase separation is followed with time elapsed and could be adjusted by storage temperature. Gelatin extracted from tilapia scale is an applicable wall material in microencapsulation and the microcapsule has real potential to be used in pharmaceuticals and cosmetic industry.

Keywords: Controlled-release, Gelatin, Tilapia, Scale, Microencapsulation, Transglutaminase, Ascorbic acid.

INTRODUCTION

Tilapia is potential to become the most important aquaculture species in the world¹ that has been widely found in tropical and subtropical areas. In 2010, the world production of farmed tilapias reached 3.2 million metric tons and about 35% was produced in China. Scale as processing waste makes up approximately 1 % of the total weight of the processed fish. Rational utilization of its processing waste plays an important role in environmental protection and comprehensive utilization. Fish scale is rich in collagen and can be a resource to extract the gelatin². Nowadays, the main resource of gelatin is still the land mammal, but the development of fishes as new resources of gelatin in the last decade is attractive³⁻⁵. There are many reasons for this tendency, apart from the well-known socio-culture and sanitary aspects and spread of disease such as bovine spongiform encephalopathy in pigs and cattle⁶, the rising interest in putting by-products from fish industry to good use is another most important reason^{7,8}. Even though there are many researches on properties of gelatin extracted from fish⁹⁻¹², which concluded that properties of gelatin from cold water fish⁷ are worse than mammalian gelatin's while properties of gelatin from warm water fish are kind of similar to mammalian gelatin's^{13,14}. However, there is few application of fish gelatin neither

cold water's nor warm water's. It is worth well to find the application area of fish gelatin that could get its maximum benefit.

Microencapsulation is an effective way to wrap active material¹⁵, which known as core material by microcapsules and it has potential to extend applications of these active materials¹⁶. Gelatin has been used as wall material in microencapsulation for a long time. We took a preliminary experiment and found that gelatin extracted from tilapia scale (FSG) would bring a higher encapsulation rate than mammalian gelatin (MG) in embedding ascorbic acid. Ascorbic acid has a broad spectrum of beneficial activities¹⁷ but its rapid degradation in aqueous solution is still a major drawback in practical application. Microcapsule could provide a protective wall for ascorbic acid, so that ascorbic acid could be effective in a relatively long time and be released when necessary.

Thus, the objective of this study is to develop gelatin extracted from tilapia scale as wall material to embedding ascorbic acid. In order to maximize the encapsulation rate of ascorbic acid microcapsule made with 15 mg/mL FSG, the relationship of factors including concentration of transglutaminase (TG) as cross-linking agent and ascorbic acid as core material, amount of AEO-9 as emulsifier and temperature of solidification between encapsulation rate are discussed. The particle size and stability of microcapsules are important for

the application of microcapsule, hence, the morphology and particle size distribution of the capsules prepared with FSG were characterized. Furthermore, controlled-release of ascorbic acid from the capsules was also detected at 5, 25 and 37 °C, respectively for further application of the microcapsule.

EXPERIMENTAL

The dried scale of tilapia was obtained from Hainan Golden Spring Food Co., Ltd (Haikou, China). Ascorbic acid was purchased from Guangzhou chemical reagent factory (Guangzhou, China). Transglutaminase (TG) was obtained from Nan Ning Pangbo Biological Engineering Co., Ltd (Nanning, China). Mammalian gelatin (MG) was purchased from Tianjin Funchen Reagents Factory (Tianjin, China). Polyoxyethylene fatty alcohol (AEO-9) was purchased from Guangzhou Kanghong Chemical Co., Ltd (Guangzhou, China). Liquid paraffin was chemical grade. All other solvents used in the study were of analytical grade.

Extraction of tilapia scale gelatin: 300 g dried scale of tilapia was immersed in 1500 mL 30 % HCl solution for 15 min with occasionally stirring. And then the scale was immersed in 1000 mL 0.1 M NaOH for 12 h under magnetic stirring. The steps above were to remove impurities including ash, fat and other protein. And after each immersing, the fish scale would be washed with tap water until the pH of the washing fluid to be 7. Next, drying the surface of fish scale before it was mixed with 1600 mL distilled water at temperature 95 °C for 3 h. The extracted solution was collected by vacuum pump and filler and then being freeze dried for later experiment.

Preparation of microcapsules: The initial condition for preparing microcapsules was described below. 1 mL of solution containing gelatin (15 mg/mL) and ascorbic acid (7.5 mg/mL) was injected into the solution formed with liquid paraffin (20 mL) and AEO-9 (100 µL). Ultrasound could help to obtain a narrower size distribution and higher microencapsulation yield¹⁸, so the study take ultrasonic cleaner (XO-520DTD) to vibrate the mixture for 10 min, while the temperature was controlled under 25 ± 1 °C. Then, the pH of the mixture was adjusted to about 6.0 by 10 % NaOH before adding 1 mL of TG (0.1 g/mL) by injection taking the most appropriate pH of TG into consideration¹⁹. Next, 30 mL 50 % ethanol was added to the mixture by injection too. Each injection took 10 s with 1 min of magnetic stirring. After these steps, the solution was put into a temperature-controlled water bath for 3 h at 40 °C (temperature of solidification). This step was needed by both the TG to cross-link gelatin and the liquid paraffin to stratify completely. Subsequently, the top layer containing liquid paraffin was removed and 10 % NaOH was added to the rest of solution until the pH came to 10 which was hold within 10 min to inactivate the TG. After that, the pH of the liquid was adjusted to about 7 with 10 % acetic acid for the storage and usage. So much for that, the microcapsules has been prepared.

For a better encapsulation rate, the factors of the concentration of TG (0, 0.05, 0.1, 0.15 and 0.2 g/mL), the volume of the emulsifier (0, 50, 100, 150, 200 µL), the concentration of ascorbic acid (3.75, 7.5, 11.25, 15 mg/mL) and temperature of

solidification (20, 40 and 60 °C) were discussed on the base of the initial condition. And each factor is investigated according to the results of the previous factors and providing a foundation for the next one. The condition that could obtain the highest encapsulation would be optimized by orthogonal test [$L_9(3^4)$] for further research.

Encapsulation rate: The encapsulation rate was determined as a function of the difference between the total mass of ascorbic acid added to the preparing solution and that being detected ascorbic acid outside microcapsules. 1 mL microcapsule solution was dialyzed against 20 mL distilled water with dialysis membrane (MWCO 8000-14000, flat width: 34 mm, Solarbio) for 24 h at 5 °C in a light-resistant container. Then the content of ascorbic acid in the 20 mL water was determined by phosphomolybdic acid colorimetry²⁰. The standard curve of ascorbic acid is $A_{760} \text{ nm} = 0.0025x + 0.0005$, $R^2 = 0.9990$. Where x is the mass of ascorbic acid (µg) in the sample and $A_{760} \text{ nm}$ was the absorbance of sample at 760 nm. Therefore, the encapsulation rate of the microcapsules could be calculated using the equation below. $W = (1 - 20 M/M_0) \times 100 \%$, where W was the encapsulation rate (%), M_0 was the total mass of ascorbic acid (µg) added in 1 mL of the microcapsule solution and $20 M$ was the mass of ascorbic acid in the 20 mL distilled water.

Morphological characteristics of microcapsules: Optical microscopy was recorded by an Olympus BX41TF microscope. For the further investigation, the solution of microcapsule was concentrated by vacuum concentrator at 45 °C until the volume into a third. Then it was dried by spray dryer (YC-015, China) with inlet air temperature of 230 °C and outlet air temperature of 93.9 °C. The obtained microcapsule's powder was white. After metal spraying process, the dried microcapsules were characterized by scanning electronic (SEM) microscopy (S-3000N, Hitachi, Japan).

Particle size analysis: The laser diffraction particle analyzer (Winner 2000, China) was used to determine the particle size and size distribution without sedimentation medium. And 10s of ultrasonic treatment for the microcapsules has hardly any influence on the analysis results.

Controlled-release characteristics of microcapsules: The solution of microcapsules was stored in a light-resistant container. For the microcapsules under storage temperature of 5 and 25 °C, the encapsulation rate was determined every day in 30 days respectively. Both of ascorbic acid and FSG are potential to be applied in human being's cosmetic and pharmaceutical, hence, the human being's body temperature was taking into consideration on the controlled release properties. Encapsulation rates of samples stored at 37 °C were determined every hour in 10 h too.

RESULTS AND DISCUSSION

Analysis of encapsulation rate: Transglutaminase cross-links protein chains through the formation of the covalent linkages between γ -carboxamide groups of peptide-bound glutamine residues and ϵ -amino groups of lysine²¹. Transglutaminase was added after the initially forming of microcapsules, so it was conjectured that the transglutaminase acted like a lock to prevent the release of ascorbic acid from the

initially formed microcapsules. In order to evaluate whether the cross-linking action of TG would affect the encapsulation rate, we performed the experiment with different concentrations of TG. The relationship between TG and encapsulation rate showed in Fig. 1a. It indicated that the cross-linking would affect the encapsulation rate. And for the concentration of TG, from 0 to 0.1 g/mL, the encapsulation rate increased with the increasing of the TG concentration, but when the TG concentration exceeded 0.1 g/mL, the encapsulation rate maintained around 74.32 %. This phenomenon supported the deduction above. Thus, the concentration of TG would not improve the encapsulation rate, but help to prevent the ascorbic acid leaking from the formed wall of gelatin. When the concentration of TG came to 0.1 g/mL, it was close to the critical value that gelatin need for the formed wall of microcapsules being cross-linked. Thus, 0.1 g/mL TG was the suitable concentration in this test. AEO-9 is nonionic surfactants with high surface activity which is a compound of amphipathic structure and does not dissociate into ions in water. Thus, the solution of AEO-9 has low surface tension and low critical micelle concentration²². However, too little emulsifier is not enough for the gelatin to adsorb in the solution and it will lead to an unstable system, while too much of emulsifier would bring out a stable system, at the same time, it would generate a great deal of

foam. Therefore, the proper amount of emulsifier used in the process should be discussed. The results presented in figure 1b and the proper amount of emulsifier was 150 μ L with the highest encapsulation rate of 76.60 % in this part. The relationship between the ratio of FSG to ascorbic acid and encapsulation rate indicated that 15 mg/mL of FSG could get a better encapsulation rate when the concentration of ascorbic acid was 7.5 mg/mL (Fig. 1c). The concentration of FSG and ascorbic acid was lower comparing to the mass production (produced with 5 % gelatin and 1.1 % sodium alginate w/v)²³, but it also need to be researched about the amount of ascorbic acid that could be embedded so that a high efficiency microcapsules could be produced. It turned out that 15 mg/mL of FSG with 7.5 mg/mL ascorbic acid could obtained the most efficiency microcapsule in this section. Solidification temperature was to provide a adapt environment for the TG to cross-link FSG. Fig. 1d presented that the solidification temperature has a big effect on the encapsulation rate too. And the encapsulation reached the better level at 40 °C which in line with the results concluded by Nielsen²⁴. The results above was optimized by orthogonal experiment with four factors and three levels [$L_9(3^4)$]. It indicated that the way to preparing the micro-capsules has advantages of simple and easily-controlled process with good repeatability. And the finally condition for the process

Fig. 1. Relationship between factors and encapsulation rate (a: Emulsifier, b: TG, c: AA, d: Temperature; Data are presented as mean $\pm$ SD (n = 3))

of preparing the microcapsule with an encapsulation of 81.17 % was 15 mg/mL FSG, 7.5 mg/mL ascorbic acid, 0.12 mg/mL TG, 150 μ L AEO-9 and 40 °C solidification temperature.

To test whether the FSG has advantage in encapsulation rate than mammalian gelatin, the mammalian gelatin was used to prepare ascorbic acid microcapsules under the optimized condition. The results indicated that mammalian gelatin only obtained microcapsules with encapsulation of 43.5 % which was lower than the 81.17 %. Therefore, the FSG was promising in microencapsulation technology, but the essence of the difference between mammalian gelatin and FSG need further investigation.

Morphology and particle size of microcapsules: The morphologies of the obtained microcapsule made with FSG in solution were manifested in Fig. 2A. All the microcapsules observed by Olympus BX41TF were small spheres and although some microcapsule possessed a particle sizes larger than 20 μ m, the main distribution of particle size of the obtained microcapsules was under 10 μ m. Fig. 2B, 2C, 2D were close-up shots of different part of Fig. 2A.

Fig. 2. Morphology of the microcapsules by microscope

The average particle size of the microcapsule was 5.73 μ m and 50 % of the microcapsules owned the particle size were less than 4.83 μ m (Fig. 3). Generally speaking, the particle size distribution of the microcapsules was focused on 4 to 8 μ m which was adapted to many applications such as cosmetic and pharmaceutical. After 30 d at room temperature, the average particle size became to be 5.47 μ m which closed to the initial value. It indicated that the structure of the microcapsules were stable.

Powder of the microcapsules was obtained by spray drying was observed by SEM and the result showed in Fig. 4. Almost all the surface of the microcapsules in Fig. 4 was folded which was formed during the spray-drying process because of the pressure within the microcapsules²⁵. On the whole, the particle size range of the microcapsules was similar to the results in Fig. 3.

Fig. 3. Morphology of the microcapsules by SEM

Fig. 4. Particle sizes of the microcapsules

Controlled-release of ascorbic acid: The encapsulation rate of ascorbic acid was changing with time under different temperature in different rates as shown in Fig. 5. As the increasing of temperature, the releasing rate was increasing. In 30 d, the encapsulation rate was 43.5 and 4.7 % at 5 °C and 25 °C, respectively. 37 °C was close to the temperature of human beings, so the controlled-release quality of microcapsule at 37 °C was promising in cosmetic and pharmaceutical industries and deserved to be investigated further more. In the article of Wang *et al.*²⁶, it took 3 h and 6 h when the cumulative release of ascorbic acid came to 50 % at 37 °C for the microcapsule with 0.48 g ascorbic acid and 0.24 g ascorbic acid, respectively. For the microcapsule made in the paper, it took 3 h at 37 °C, the cumulative release of ascorbic acid came to 35 %, equaled to the encapsulation rate of microcapsules in 10 d at 25 °C and in 22 d at 5 °C. And it also took about 6 h and 15 d and 30 d came to the cumulative release of ascorbic acid at 37, 25 and 5 °C.

Conclusion

This study suggests that tilapia scale might be successfully used in gelatin production, giving relatively high encapsulation

Fig. 5. Changes of encapsulation rate with time at different temperatures (Data are presented as mean $\pm$ SD (n = 3))

rate in microencapsulation technology. According to the experiment, the optimum preparation conditions were found to be 15 mg/mL FSG, 7.5 mg/mL ascorbic acid, 0.12 mg/mL TG, 150 μ L AEO-9 and 40 °C solidification temperature. This condition could obtain the microcapsules with encapsulation rate of 81.17 % and average particle size of 5.73 μ m. This promising property could create significant demand for tilapia gelatin which might then be used widely to replace commercial mammalian gelatin. Further study on the essence of the difference between the commercial gelatin and FSC in the application of microencapsulation technology will be carried out. The controlled-release properties of the microcapsule at 5, 25 and 37 °C might then be used widely in food, cosmetic and pharmaceutical industries.

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REFERENCES

1. J. Thodesen (Da-Yong Ma), M. Rye, Y.-X. Wang, K.-S. Yang, H.B. Bentsen and T. Gjedrem, *Aquaculture*, **322-323**, 51 (2011).
2. F. Zhang, S. Xu and Z. Wang, *Food Bioprod. Process.*, **89**, 185 (2011).
3. H. Yang and Y. Wang, *Food Hydrocoll.*, **23**, 577 (2009).
4. H.S. Tabarestani, Y. Maghsoudlou, A. Motamedzadegan and A.R. Sadeghi Mahoonak, *Bioresour. Technol.*, **101**, 6207 (2010).
5. M.H. Norziah, A. Al-Hassan, A.B. Khairulnizam, M.N. Mordi and M. Norita, *Food Hydrocoll.*, **23**, 1610 (2009).
6. S.S. Choi and J.M. Regenstein, *J. Food Sci.*, **65**, 194 (2000).
7. M.C. Gómez-Guillén, J. Turnay, M.D. Fernández-Díaz, N. Ulmo, M.A. Lizarbe and P. Montero, *Food Hydrocoll.*, **16**, 25 (2002).
8. A.A. Karim and R. Bhat, *Food Hydrocoll.*, **23**, 563 (2009).
9. T. Nagai, *Food Chem.*, **68**, 277 (2000).
10. S. Benjakul, K. Oungbho, W. Visessanguan, Y. Thiansilakul and S. Roytrakul, *Food Chem.*, **116**, 445 (2009).
11. N.F. Mohtar, C. Perera and S.-Y. Quek, *Food Chem.*, **122**, 307 (2010).
12. S. Wangtueai and A. Noomhorm, *LWT-Food Sci. Technol.*, **42**, 825 (2009).
13. K. Piez and J. Gross, *J. Biol. Chem.*, **254**, 995 (1960).
14. A.I. Sarabia, M.C. Gómez-Guillén and P. Montero, *Food Chem.*, **70**, 71 (2000).
15. H. Umer, H. Nigam, A.M. Tamboli and M.S.M. Nainar, *Int. J. Res. Pharm. Biomed. Sci.*, **2**, 474 (2011).
16. W. Li, G. Wu, H. Chen and M. Wang, *Colloids Surf. A*, **333**, 133 (2009).
17. K.L. Keller and N.A. Fenske, *J. Am. Acad. Dermatol.*, **39**, 611 (1998).
18. K. Makino, T. Mizorogi, S. Ando, T. Tsukamoto and H. Ohshima, *Colloids Surf. B*, **22**, 251 (2001).
19. R.-N. Chen, H.-O. Ho and M.-T. Sheu, *Biomaterials*, **26**, 4229 (2005).
20. E.Y. Backheet, K.M. Emara, H.F. Askal and G.A. Saleh, *Analyst*, **116**, 861 (1991).
21. K. Yokoyama, N. Nio and Y. Kikuchi, *Appl. Microbiol. Biotechnol.*, **64**, 447 (2004).
22. G. Jing, T. Chen and M. Luan, *Arabian J. Chem.*; doi:10.1016/j.arabjc.2011.06.007.
23. S. Sakai, S. Ito and K. Kawakami, *Acta Biomater.*, **6**, 3132 (2010).
24. P.M. Nielsen, *Food Biotechnol.*, **9**, 119 (1995).
25. T.-Y. Ting, I. Gonda and E. Gipps, *Pharm. Res.*, **9**, 1330 (1992).
26. H. Wang, H. Shi, A.C. Cheung and J.H. Xin, *J. Control. Rel.*, **152**(Suppl. 1), e78 (2011).